## "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

ZHBANKOV, B.V.; SIDOEOV, B.M.

Automatic single-chain OAE elevator for bottle conveying between floors. Trudy UkrNIISP no.9:145-150 '64. (MIRA 17:10)

USTIMENKO, V.F., starshiy dorozhnyy master; ZYKOV, F.M., starshiy dorozhnyy master; KIREY, P.I.; IVANITSKIY, M.V.; LOBANOV, Ye.I., dorozhnyy master; GAYDAR, P.R.; SIDOBOV, B.N.; SAVKOV, Ye.I.; SAPONKIN, A.N.; PETROV, A.S.; BURLAK, F.V., inzh.

Letters to the editor. Put' i put.khoz. 5 no.5:42-44 My '61.

(MIRA 14:6)

1. Stantsiya Kupino, Onskoy dorogi (for Ustimenko). 2. Stantsiya Kotel'nich, Gor'kovskoy dorogi (for Zykov). 3. Stantsiya Petropavlovsk, Omskoy dorogi (for Kirey, Ivanitskiy). 4. Stantsiya Stupino, Moskovskoy dorogi (for Lobanov). 5. Zamestitel' nachal'—nika distantsii puti, st., Izyum, Donetskoy dorogi (for Gaydar).

6. Machal'nik distantsii puti, st. Berlik, Kazakhskoy dorogi (for Sidorov). 7. Nachal'nik PMS-62, st. Nikitovka, Donetskoy dorogi (for Savkov). 8. Smennyy master shchebenochnogo kar'yera st. Chokpar, Kazakhskoy dorogi (for Safonkin). 9. Nachal'nik tekhnicheskogo otdela slushby puti, g. Yaroslavl' (for Petrov).

10. Distantsiya zashchitnykh lesonasazhdeniy, st. Artemovsk, Donetskoy dorogi (for Burlak).

(Railroads)

SIDOROV, B.N. (Alma-Ata)

Improving the organization of work. Put' i put.khoz. 8 no.4:12-14 '64. (MIRA 17:4)

SHAPOSHNIKOV, V.N., akademik, redaktor; KONDRAT'YEVA, E.N. [translator]; MEKRTIYEVA, V.L. [translator]; SIDOROV, B.N., redaktor; ENDEN, M.G., redaktor; SHAPOVALOV, V.I., tekhnicheskiy redaktor

[Bacterial physiology. Translated from the English] Fiziologia bakterii. Perevod s angliiskogo E.N.Kondrat'evoi i V.L.Mekhtievoi. Pod red. i s predisl. V.N.Shaposhnikova. Moskva, Izd-vo inostrannoi lit-ry, 1954. 547 p. (MIRA 7:11) (BACTERIA)

. SIDOROV, B.N.; KHVOSTOVA, V.V.

Factors influencing the genetic effect of ionizing radiations.

Itogi nauki: Biol. nauki no. 3:176-227 160. (MIRA 13:10)
(RADIATION—PHYSIOLOGICAL EFFECT) (VARIATION (BIOLOGY))

DUBININ, N.P.; SIDOROV, B.M.; SOKOLOV, N.N.

Experimental analysis of the primary mechanism of the effect of radiation on cell nuclei. Dokl.AN SSSR 133 no.1:221-224 J1 '60. (MIRA 13:7)

1. Institut biofiziki Akademii nauk SSSR. 2. Chlen-korrespondent AN SSSR (for Dubinin).

(RADIATION--PHYSIOLOGICAL EFFECT)

(CHROMOSOMES)

'SIDOROV, B.N.; DUBININ, N.P.; SOKOLOV, N.N.

Experimental study of the mole of free radicals and the direct effect in the primary mechanism of the radiation effect. Radiobiologia 1 no.2:161-171 '61. (MIRA 14:7)

1. Institut biologicheskoy fiziki AN SSSR, Moskva.
(RADICALS (CHEMISTRY))
(RADIATION—PHYSIOLOGICAL EFFECT)

33315

S/560/61/000/010/013/016 D299/D302

27. 1220

.

Sidorov, B. N., and Sokolov, N. N.

TITLE:

AUTHORS:

Effect of space-flight conditions on the seeds of Allium Fistulosum (winter onion) and Nigella

Damascena (ranunculus)

SOURCEs

Akademiya nauk SSSR. Iskusstvennyye sputniki

Zemli. no. 10. Moscow, 1961, 93-95

TEXT: Dry seeds of the radicsensitive A. fistulosum and of the radiostable N. damascena were investigated. From a table, it is evident that the A. fistulosum is 9 times more sensitive to X-rays than the N. damascena. A comparison of the number of aberrations in the seeds which took part in the flight with control seeds showed no difference whatsoever in the frequency of chromosome rearrangements in the seeds under investigation. This negative result, obtained with dry seeds, made it necessary to conduct tests with growing seeds. These tests showed that

Card 1/3

33315 S/560/61/000/010/013/016 D299/D302

Effect of space-flight ...

space-flight conditions have a stimulating effect on the growth of both species; this stimulating effect is more noticeable in the radiostable species N. damascena. In general, dry seeds are fairly stable to ionizing radiation; thus, the seeds of A. fistulosum have to be irradiated by a dose of 250 - 500 r, and those of N. damascena by several thousands of röntgen in order to observe an actual increase in chromosome rearrangements. The authors arrive at the conclusion that the increase in the growth of the seeds cannot be related to stimulating radiation doses, as the stimulating effect is stronger in the radiostable species N. damascena and weaker in the radiosensitive species A. fistulosum. If the observed effect on the N. damascena would have been due to radiation, the indicated dose would have caused chromosome aberrations in the A. fistulosum too. This was, however, not observed. It is evident that the reason for the observed effect should be sought in other factors which are active in space-flight--factors which are thoroughly unlike those

Card 2/3

SIDOROU, 13.10. Correlation Between the Redox Potential of the Lymph of Crickets During tradial on and Radiosensitivity

G. V. SumarCanv

A nucromethod has been developed to determine the redox potential of the harmolymph of inects in viro. The effect of various protective factors (hypoxia, protective substances) which influence the radiomensisting of insects has been investigated.

Uncertedated differences in the values of the redox potential have been observed for solutions of protective substances and for tissues into which protective substances had been introduced. On the other hand, when protective substances are introduced into the regainst during hypoxia, the values of the redox potential exactly correlate with the magnitude of the protective effect and radiomensitivity. The data reported in the literature which failed to show such correlation were obtained when the potential was measured in viro and did not allow for the redistribution of the rates of oxidation-reduction reactions in living systems, altered by the protective effects.

Liminatore State Consectiv, Marcon, USSR

Direct and Indirect Radiation

N. P. Dubinin, B. N. Sidorer and N. N. Sekoler

It is known that molecules in aqueous solution can undergo radiochemical reactions due to free radicals from the radiolysis of water, or by direct energy absorption.

The genetic effectiveness of free radicals produced chemically within the cell tFenton reaction, reaction of accorbic acid with hydrogen perovide) allows us to assets the importance of the direct and indirect radiation effects on chromosomes. It was shown in plar t cells (rootlets of Allium Intulatum) that substances which protect the chromosomes from the effect of the free ra heals OH and HO, obtained chemically (K, KB, hyposulphite, etc.) are not protective when the chromosomes a v irraduated with X-rays. We conclude that the genetic effect of radiation is due mainly to the direct effect and not to the products of water radioly is.

Parallel experiments with DNA solutions (M. I. Mekshenkov) showed that the effectiveness of the direct action on DNA is much greater than that of the indivect effect.

The considerable protective ability of substances which protect chromosomes from free radions was demonstrated in solutions of DNA only at low DNA concertrations. In solutions with high DNA concentrations the protective effect is virtually absent which points to the predominant rôle of the direct effect.

Institute of Stophysics, Academy of Telences of the USSA, Moscow

report presented at the 2nd Intl. Congress of Radiation Research, Harrogate/Iorkshire, Gt. Brit. 5-11 Aug 1962

SIDOROV, B.N.: SOKOLOV, N.N.

Effect of the conditions of space flight on the seeds of Allium fistulosum and Nigella dammscena. Probl.kosm.biol. 1:248-251 '62. (MIRA 15:12) (SPACE FLIGHT--PHYSIOLOGICAL EFFECT) (SEEDS)

KHVOSTOVA, V.V.; PROKOF YEVA-BEL GOVSKAYA, A.A.; SIDOROV, B.N.; SOKOLOV, N.N.

Effect of the conditions of space flight on the seeds of higher plants and on actinomyces. Probl.kesm.biol. 2:153-163 '62.

(MIRA 16:4)

(SPACE FLIGHT—PHYSIOLOGICAL EFFECT)
(PLANTS, EFFECT OF SPACE FLIGHT ON)
(ACCINOMYCES)

SIDOROV, B.N.; SOKOLOV, N.N.

Radiation analysis of chromosome discreteness during the process of autoreproduction. Radiobiologia 3 no.3:415-419 163. (MIRA 17:2)

1. Institut biologicheskoy fiziki AN SSSR, Moskva.

### "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

Lysis of chromosomes and the blockade of the spindle. Biul.
MOIP. Otd. biol. 68 no.5:78-91 S-0 '63. (MIRA 16:10)

SIDOROV, B.N.; SOKOLOV, N.N.

Lysis of the chromosomes accompanying spindle blockade. Dokl. AN SSSR 150 no.3:653-656 My '63. (MIRA 16:6)

1. Institut biologicheskoy fiziki AN SSSR. Predstavleno akademikom V.N. Sukachevym.
(Chromosomes) (Karyokinesis)

SIDOROV, B.N.; SOKOLOV, M.F.; ADDREYEV, V.S.

Mutagenic effect of etiglenimine in a rories of cell generations.

Genetika no.1:112-122 165. (MIPA 18:10)

1. Institut biologicksokoy fiziki AN SSSE, Moshva.

SIDOROV, B.N.; SOKOLOV, N.N.

Radiation arelysis of the structure and reproduction of chromosomes. Radiobiologia 4 no.6:828-835 '64. (MIRA 18:7)

1. Institut biologicheskoy fiziki AN SSSR, Moskva,

SIDOROV, B.N.; SOKOLOV, N.N.

Spindle blocking as a cause of the formation of rolymorphous nuclei in polyploid cells. TSitologiia 7 no.5:645-650 S-0 '65.

1. Laboratoriya radiatsionnoy genetiki Instituta biofiziki AN SSSR, Moskva. Submitted August 10, 1964.

#### "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

Draft of new norms for determining costs of machinery spare parts.
Stroi. truboprov. 5 no.10:29 0'60. (MIRA 13:10)
(Building machinery-Equipment and supplies)

# "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

Amortization allowances for machines. Stroi. truboprov. 6 no. 2:25 f :61. (MIRA 14:5)

SIDOROV, B.S., inzh.

Economic basis for choosing pipe-carrying machinery. Stroi. truboprov. 7 no.7:28-29 Jl '62. (MIRA 15:7) (Pipe-Transportation)

### "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

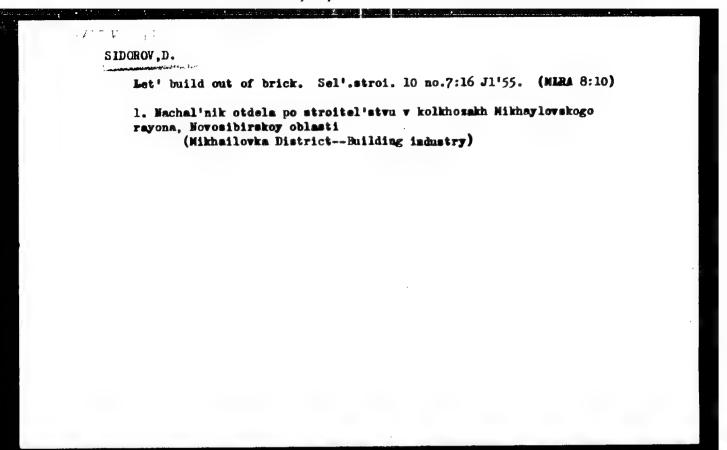
SEMENOV, B.N., kand.tekhn.nauk; SIDOROW, B.S., inzh.

Study of the efficiency of using transportation facilities for moving pipes. Trudy VNIIST no.14:114-123 '62. (MIRA 16:12)

SIDOROV, B.S., insh.

New standards for amortization deductions for machinery in pipeline construction. Trudy VNIIST no.14:105-113 '62.

Technical and economic analysis of the efficiency of machines for cleaning pipes with a diameter of 720 and 820 . Ibid. \$164-168 (MIRA 16:12)



Repairing metal bridge spans. Put' i put. khoz. no.9:18 S '58.

(MIRA 11:9)

1. Nachal'nik otdela inzhenernykh sooruzheniy, Leningrad.

(Railroad bridges---Maintenunce and repair)

#### "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

SIDOROV, D.A., inzh.

New method for repairing abutments. Put' i put. khoz. no.5:19-20
My '59.

(Railroads—Maintenance and repair)

(Railroads—Maintenance and repair)

Control Ministration (April 1984) And the Control of Manager (April 1984) And the Control of Contro

VOLKOV, P.F.; SIDOROV, D.A.

Remedial treatment of embankments. Put' i put.khoz. 4 no.6:19
Je '60. (MIRA 13:7)

1. Starshiy inzhener distantsii puti, stantsiya Chudovo, Oktyabr'skoy dorogi (for Volkov). 2. Nachal'nik otdela inzhenernykh sooruzheniy sluzhby puti, stantsiya Chudovo, Oktyabr'skoy dorogi (for Sidorov).

(Embankments--Maintenance and repair) (Railroads--Track)

SIDOROV, D.A., insh. (Leningrad); POMOGAYEV, P.Ye., insh. (Leningrad)

Maintenance and repair of mansive bridge substructures. Put'
i put. khos. 4 no. 12:28-29 D '60. (MEA 13:12)

(Railroad bridges—Maintenance and repair)

### "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

Think of bear.

Subject : USSR/Electricity

AID P - 1943

Card 1/1 Pub. 29 - 23/31

Authors : Yecheistov, N. K., and Sidorov, D. F., Engs.

Title : Complete apartment panelboard

a management of the second of

Periodical: Energetik, 3, 28-29, Mr 1955

Abstract: The authors describe the panelboard designed by the design division of the city's Metro Transportation

System. They give all data concerning dimensions, equipment, and performance. One detailed drawing with

connections diagram.

Institution: None

Submitted: No date

YECHEISTOV, N.K., inzhener; SIDOROV, D.F., inshener.

Complete apartment electric control box having three circuits, a meter and safety fuses. Gor. khoz. Mosk. 29 no.5:38 My '55.

(Wattmeter) (Blentric fuses) (NLRA 8:6)

SIDOROV, D.P., inshemer.

Heek for uprecting tree stumps. Terf.prem.33 me.5:35-36 \*\*156.

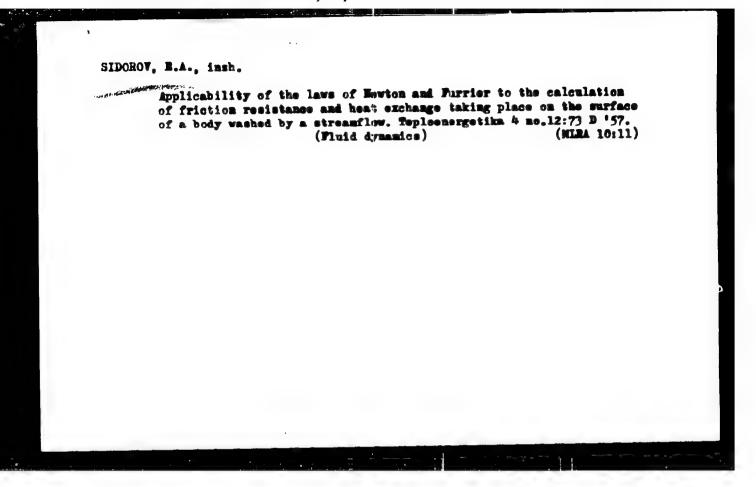
(MLRA 9:9)

1.Shaturskeye terfepredpriyatiye.

(Heeks) (Clearing of lands)

Stratigraphy of Mesozoic coal-bearing sediments in the Ust'-Vilyuy gas-bearing region. Trudy VNIGRI no.186:32-43 '61. (MIRA 15:3)

(Verkhoyarsk Range--Coal geology)



#### "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

AUTHOR:

SIDOROV, E.A.

PA - 2128

TITLE:

On the Consideration of the Influence exercised by the Non-Isothermal Flux in a Laminar Current of Liquids which are Capable of Dripping in Tubes.

PERIODICAL:

Zhurnal Tekhn. Fiz., 1957, Vol 27, Nr 2, pp 327 - 330 (U.S.S.R.).

Received: 3 / 1957

Reviewed: 4 / 1957

ABSTRACT:

The object of the present work is to find an approximative equation for the field of velocity and the temperatures in the case of a laminar current in tubes with liquids which are capable of dripping in consideration of the changing of the viscosity of the liquid with respect to temperature. This investigation was undertaken for the purpose of showing that the modification of the physical characteristics of liquids with temperature is one of the most important causes of the divergence between theoretical solutions and experimental results. At first the equations for the motion and heat transfer in the boundary layer of cylindrically shaped tubes are written down. The existing solutions of this system of equations apply only to the case of m = const, which leads to more or less grave errors. Therefore, the attempt was made to find an approximated solution for this system of equations for the case that the change of the viscositymin connection with temperature is taken into account. The method of successive approximation by SHVETS-TARGA was selected for this purpose. At

Card 1/2

PA - 2128 On the Consideration of the Influence exercised by the Non-Isothermal Flux in a Laminar Current of Liquids which are Capable of Dripping in Tubes.

first, temperature distribution in first approximation for the radial cross section of the boundary layer of the tube was found. Next, the temperature dependence of the viscosity coefficient of the liquid capable of dripping is shown with the required accuracy in form of a series. In practice the polynomial of the third, or even only of the second degree will suffice. After transformation and integration the equation for the velocity of the flux in the case of a nonisothermal motion in the tube is obtained. Next, the formula for the average velocity of the cross section is given, after which only the domain adjoining the wall is investigated and the equation is found in which one of the multiplicands takes the influence exercised by the non-isothermal course of the current into account. In the case of the second initial equation the case of an infinite distance from the wall is dealt with and an ordinary differential equation is obtained. The average value of the heat current passing through the unit of the surface of the tube is written down in form of a formula.

Card 2/2

ASSOCIATION: Not given

PRESENTED BY: SUBMITTED:

AVAILABLE:

Library of Congress.

SINCE CA, A

AUTHOR TITLE

PA - 2547 On the Correlation between Surface Friction and Heat Exchange. (O svyazi poverkhnostnogo treniya s teplochmenom.- Russian)

PERIODICAL

Zhurnal Tekhn. Fiz. 1957, Vol 27, Nr 3, pp 560 - 566 (U.S.S.R.)

ABSTRACT

Though the theory on the analogus phenomena on the occasion of Received: 4/1957 the transmission of momenta and energy in relation to the quantitative part, which was for the first time mentioned by Reynolds, was named the hydrodynamic theory of heat exchange, the author believes that it ought to be called the theory of thermefriction analogy. The reason given for this is that the main task of this theory is the discovery out of a direct relation between the hydrodynamic and the heat exchange characteristics. Existing methods are not complete and results differ up to 100 % and more. A much mere simple and safe way is shown here. At first the universal relation between Nu and Re is deduced:

$$Nu = \frac{1}{2} c_f Re \left(\frac{\mathbf{Q} \cdot \mathbf{Q}}{\Im \varphi}\right)_0$$

$$\theta = \frac{t}{t_0}$$
 .....dimension/less temperature

CARD 1/2

APPROVED FOR RELEASE: 08/23/2000

CIA-RDP86-00513R001550510007-7"

PA - 2547

On the Correlation between Surface Friction and Heat Exchange.

The value ( ) here acts as second parameter. The determination of this value ( ) here acts as second parameter. The determination of this value ( ) here acts as second parameter. The determination of this value value of this parameter can be assumed to differ only little from that of the laminary boundary layer. This value can be found analytically for the laminary boundary layer. It is derived here and the basic equation reads as follows:

 $Nu = \frac{1}{2} c_{\mathbf{f}} Re Pr 1/3_{\mathbf{v}}$ 

Now this formula for the different cases of a turbulent flow is applied and it is shown that the results obtained agree with those of the experiments. The same is shown to be the case with motions of liquids in tubes as well as with the motions of a compressed gas. The last mentioned formula remains the same for gases. (With 2 tables)

ASSOCIATION: not given.

PRESENTED BY: -

SUBMITTED: June 30th, 1956.
AVAILABLE: Library of Congress.

SIDOCOV, E.A., Gand Tech Sci -- (diss) "Certain problems of the theory of convective and radial heat exchange."

Mos, Fub House of Acad Sci USSR, 1958, 9 pp

(Acad Sci US R. Power Engineering Inst im G.V.

Krznizhanovskiy) 185 copies. List of author's works

pp 8-9 (11 titles) (KL, SC-58, 125)

- 80 -

Contemporary methods in convection heat transfer theory and their application. Inzh.-fiz.zhur. no.5:62-70 My '58. (MIRA 12:1)

1. Energeticheskiy institut AN SSSR, g. Moskva.

(Heat--Transmission)

```
SIDOROV, E.A., inzh.

A valuable book on the theory of convective heat exchange

("Foundations of the theory of heat exchange" by S.S. Eutstelsdae.

Envisewed by E.A. Sidorov). Energomashinostroenie 4 no.11:43

E *58.

(MIRA 11:11)

(Eutstelsdae, S.S.)
```

AUTHOR: Siderov, E.A. (Moscow) SOV/24-58-9-18/31

TITLE:

Convective Heat Transfer Under Non-stationary Conditions (Konvektivnyy teplochmen pri nestatsionarnom rezhime)

PERIODICAL:

Izvestiya Akademii Nauk SSSR, Otdeleniye Tekhnicheskikh Nauk, 1958, Nr 9, pp 116 - 117 (USSR)

ABSTRACT: Non-stationary convective heat transfer is met with in many branches of technology. The non-stationarity may be associated with the process itself or with a transition state from one stationary process to another. In spite of the major practical importance of non-stationary thermal convection, there are no theoretical or experimental data on the subject at the present time. The absence of such data is due to the great mathematical difficulties involved in an accurate solution of the problem. This is the reason why in calculations of heat-transfer processes in which speeds and temperatures are functions of time, one has been forced to use formulae which describe stationary convection assuming that these formulae will also apply when the speeds and temperatures which enter into them vary with time. However, there are no data in the literature which would indicate the range of applicability of these formulae. The present paper is an attempt to obtain an

Cardl/5

SOV/24-58-9-18/31

Convective Heat Transfer Under Non-stationary Conditions

approximate solution of the problem of non-stationary convection. In calculation of heat transfer between a medium in which convection takes place and a surface, the basic energy equation in a layer near the surface may be written in the form:

$$\frac{\partial t}{\partial x} + u \frac{\partial t}{\partial x} + v \frac{\partial t}{\partial y} = B \frac{\partial^2 t}{\partial y^2}$$
 (1).

Here u and v are the components of the velocity vector along the x and y axes which coincide with the direction of flow and the normal to the surface respectively,  $t = T - T_1$  is the temperature difference between a point in the layer and the surface,  $\tau$  is the time and a is the

coefficient of "temperature conductivity". In the zeroorder approximation only the conductive term is retained.
On solving the equation:

Card2/5

$$\frac{\partial^2 t}{\partial y^2} = 0 \tag{2}$$

SOV/24-58-9-18/31

Convective Heat Transfer Under Non-stationary Conditions

in which convection is taken indirectly into account via the boundary conditions:

$$t = 0$$
 for  $y = 0$ ,  $t = t_0$  for  $y = \delta$  (3)

we find:

$$t = t_0 y/\delta \tag{4}$$

where  $\delta$  is the thickness of the layer,  $t_0 = T_0 T_1$  and  $T_0$  is the temperature of the main current. Substituting this expression into Eq.(1), in which only convective terms are now neglected, we find the equation which takes into account the non-stationary nature of the phenomenon in the first-order approximation:

in the first-order approximation:  

$$y \frac{\partial}{\partial x} \left( \frac{t_0}{\delta} \right) = a \frac{\partial^2 t}{\partial y^2}$$
(5).

On solving this equation, one finds that:

Card3/5

SOV/24-58-9-18/31

Convective Heat Transfer Under Mcn-stationary Conditions

$$\frac{q}{q_o} = 1 - \frac{c \cdot \lambda t_o^2}{6q_o^2} \left( \frac{t_c'}{t_o} + m \frac{u'}{u} \right)$$
 (8)

where q is the thermal flux through the surface in the non-stationary case and  $\mathbf{q}_0$  is the flux under stationary conditions. It follows that the formulae describing the stationary process will hold appreximately provided:

$$\frac{Q \operatorname{c}\lambda}{6\alpha_{c}^{2}} \left(\frac{\mathbf{t}_{o}^{\prime}}{\mathbf{t}_{o}} + \operatorname{m} \frac{\mathbf{U}^{\prime}}{\mathbf{U}}\right) \langle \langle \underline{\mathbf{1}} \rangle \rangle$$
(10)

where  $\rho$  and c are the density and specific heat, respectively and u is the velocity of the main current beyond the layer near the surface. For laminar flow

Card 4/5

Convective Heat Transfer Under Non-stationary Conditions

m = 1/2 and for turbulent flow m = 1/5 . The prime indicates differentiation with respect to time and  $\alpha_0$  =  $q_0/t_0$  .

SUBMITTED: February 27, 1957

Card 5/5

24(8) SOV/57-58-12-10/15 AUTHOR: Sidorov; E. A. Non-Isothermicity on the Hydraulic Drag TITLE: On the Influence of in Laminar Motion of Drop Liquids in Pipes (O vliyanii neizotermichnosti na gidravlicheskoye soprotivleniye pri laminarnom dvizhenii kapel'nykh zhidkostey v trubakh) Zhurnal tekhnicheskoj fiziki, 1958, Nr 12, pp 2711-2712 (USSR) PERIODICAL: ABSTRACT: The results obtained previously in the paper cited in reference 1 are further developed, made more precise and compared with experimental data. In order to check formula (4) specifying the heat flow between the liquid and the wall of the tube the problem of the influence of the direction of a heat flow is investigated. The influence of the non-isothermic course on the hydraulic resistance is then examined. It is shown that formula (8) is a generalization of formula (9) established by Poisecille (Puazeyl') for the case of a non-isothermal motion. The relative of { (coefficient of hydraulic drag) in the case of a change in direction of the heat flow was calculated. Water was used as fluid medium and for the calculation of the coefficient of the non-isothermicity Card 1/2 formula (5) was employed. It is shown that for the hydraulic

On the Influence of Non-Isothermicity on the SOV/57-58-12-10/15 Hydraulic Drag in Laminar Motion of Drop Liquids in Pipes

drag the difference between the theoretical and experimental values does not exceed 1 %. There are 3 references 2 of which are Soviet.

SUBMITTED: December 20, 1957

Card 2/2

A Sychological &

AUTHOR: Sidorov, E. A., Engineer.

96-4-15/24

TITLE:

A method of allowing for unstable conditions during

convective heat exchange. (Uchet vliyaniya

nestatsionarnosti rezhima pri konvektivnom teploobmene).

PERIODICAL: Teploenergetika, 1958, 5 No.4, pp.79-80 (USSR).

ABSTRACT: Despite the practical importance of unstable thermal convection, the problem has been neglected. A strict theoretical solution presents great mathematical difficulties. Therefore, use is usually made of formulae appropriate to the steady state; their applicability to unstable conditions of heat exchange is assumed. However, there is as yet no way of estimating the error inherent in this assumption. The present article uses the method of successive approximations to establish a simple expression whereby the applicability of the assumption can be roughly calculated. Formulae are derived to determine the applicability of the steady

convection formulae. They are applied in a numerical example on turbulent flow in a pipe, and the use of the steady state equations is found to be admissable.

ASSOCIATION: All-Union Thermo-Technical Institute.
(Vsesoyuznyy Teplotekhnicheskiy Institut).

AVAILABLE: Library of Congress.

31582 S/124/61/000/011/023/046 D237/D305

26,5000

AUTHOR:

Sidorov, E.A.

TITLE:

Radiant and convection heat exchange in absorbing

medium

PERIODICAL:

Referativnyy zhurnal, Mekhanika, no. 11, 1961, 88, abstract 11B591 (\$b. vopr. teploobmena, M., AN SSSR,

1959, 49 - 52)

TEXT: In the energy equation of a flat laminar boundary layer of a incompressible fluid the heat gain is assumed to be due to radiation and influence of viscosity is neglected. Direction of the radiant beam is considered to be normal to the streamlined surface and the fluid is optically grey. The energy transfer equation is taken in the form averaged over direction and on its integration the approximation is assumed that inside the boundary layer the temperature is constant and equal to that of a free flow outside the boundary layer. The resulting energy equation is

Card 1/3

31582 S/124/61/000/011/023/046 D237/D305

Radiant and convection heat ...

$$\rho c \left( u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = \lambda \frac{\partial^2 T}{\partial v^2} + \epsilon m \sigma n^2 \left( T_1^4 - T_0^4 \right) e^{-my},$$

where u, v,  $\rho$ , T are velocity components, density and temperature of the fluid,  $\lambda$  - coefficient of thermal conductivity, c - heat capacity,  $T_1$ ,  $T_0$  - temperature of the surface and the fluid on the boundary of the layer,  $\varepsilon$  - coefficient of blackness (absorption) of the surface,  $\sigma$  - Stefan's constant, n - index of refraction of fluid, m = 3/2 k, k = coefficient of absorption of fluid. This equation is solved (to 1st approximation) by modified Shvetz method (Shvetz, M.Ye. Prikl. matem. i mekhan. 1950, 14, no. 1)). The solution is sought of the equation with the L.H.S. neglected, satisfying the condition of equal temperatures on the wall and on the boundary of the layer, when the thickness of thermal boundary layer  $\delta$  is the 2nd approximation obtained by Skvetz method, when radial heat transfer is neglected. Thus, the author obtains the following expression for heat transfer intensity q through the wall

Card 2/3

Radiant and convection heat ...

31.582 S/124/61/000/011/023/046 D237/I305

$$q = \frac{\lambda(T_1 - T_0)}{\delta} + \frac{q_1}{m\delta} (1 - e^{-m\delta})$$

 $q_{\uparrow}$  - intensity of incident beam on the wall. For  $k\lambda/\alpha_{0}<0.1$ , where  $\alpha_{0}$  - coefficient of heat transference, convective and radiant heat transfer are practically additive and can be calculated separately. [Abstractor's note: Complete translation].

X

24,5200 AUTHOR:

Sidorov, E. A.

68767

3/170/59/002/11/013/024

B014/B014

TITLE:

Calculation of Resistance and Convective Heat Exchange Under Turbulent Nonsteady

Conditions

PERIODICAL:

Inzhenerno-fizicheskiy zhurnal, 1959, Vol 2, Nr 11, pp 86-91 (USSR)

ABSTRACT:

Proceeding from the set of equations (1) for heat transfer under arbitrary conditions, the author derives equations (5) and (6) for equations (2) and (3). These two equations are considered to be sufficiently accurate solutions of (1). For practical purposes, however, they proved to be not very useful. The author suggests to derive less complicated and thus more useful approximate solutions. A correction of the solution for steady conditions leads to formula (9) for nonsteady conditions, which has the form of the ordinary Bernoulli differential equation. Next, formula (11) for the resistance coefficient is deduced herefrom. A similar way is chosen for equation (6) for the heat exchange. Thus, formula (20) is obtained which is used to compute the Stanton number. There are 5 references, 4 of which are Soviet.

ASSOCIATION:

Institut teplofiziki SO AN SSSR (Institute of Thermophysics SO,

AS USSR)

Card 1/1

24,5200

67604

AUTHOR:

Sidorov, E.A. (Moscow)

SOV/179-59-5-26/41

TITLE:

The Interaction of Convection and Radiation in an

Absorbing Medium

PERIODICAL: Izvestiya Akademii nauk SSSR, Otdeleniye tekhnicheskikh

nauk, Mekhanika i mashimostroyeniye, 1959, Nr 5,

pp 134-136 (USSR)

ABSTRACT:

The plane motion of an incompressible fluid with constant physical properties near a non-isothermal surface is considered. The equations for the conservation of mass and energy and for radiational transfer are written in differential form; the latter equation involves the Stefan-Boltzmann constant and the refractive index of the medium. These equations are solved by means of exponential functions to obtain the radiation transfer, which is then substituted in the energy equation. The resulting equation is solved by an iterative process for both turbulent and laminar flow to obtain the final equation for total heat transfer. There are 6 Soviet references.

SUBMITTED: July 13, 1959

Card 1/1

5/177

8/179/59/000/06/028/029 R081/E1-1

AUTHOR:

TITLE:

(Mosecu) Sidorov, B.A.

The Influence of Initial Section on the Hydraulic

Rosistance in Laminar Flow of Liquids in Tubes

PERIODICAL: Izvestiya Akademii nauk SSSR, Otdaleniya takhmichaskikin

nauk, Mekhanika i mashinostroyeniye, 1959, Nr 6,

p 150 (USSR)

ABSTRACT: Attempts to establish theoretical and experimental

corrections allowing for the influence of the initial

section of the tube have already been made by

The most accurate solution (Rafs l-1).Bussinesq giving a basis for practical recommendations on the calculation of hydraulic resistance in the initial section is the relatively recent analytical solution of S.M. Targ (Ref 4). The accuracy of the solution is

established by the very good correspondence with the experimental distribution of flow velocity in a tube found

On the basis of S.M. Targ's by Nikuradze (Ref 3).

findings, the fall in pressure of - p between the Card 1/5

section of entry (x = 0, p = p) in a circular tube and an arbitrary section distance x from the entrance can be

calculated from the change along the length of the tube of

\$/179/9/000/00/00/02/02/ \$031/\$141

The Influence of Initial Section on the Hydraulic Resistance in Laminar Flow of Liquids in Tubes

the local and the mean of the hydraulic resistance coefficient. Omitting intermediate steps, the final result can be written

$$i = \frac{dp}{dx} \frac{2d}{o0^2} = \frac{64}{R} + \frac{32}{R} \frac{co}{exp} - \frac{46k^2}{R} \frac{x}{c}$$
 (1)

'R = Ud/ ):

$$i \circ = \frac{1}{x} \int_{0}^{x} f dx = \frac{6^{1}x}{R} + \frac{2d}{x} \left[ \frac{1}{3} - 4 \int_{k=1}^{\infty} \frac{1}{6k^{2}} exp \left[ -\frac{13k^{2}}{R} \frac{x}{d} \right] (2)$$

where R is Reynold's number; U the mean flow velocity; d the equivalent diameter of the tube; I and o respectively the kinematic viscosity coefficient and density of the moving fluid; and  $\beta_K$  ( $k=1,2,3,\ldots$ ) the successive roots of the equation  $I_2(z)=0$ . If the second term of the formulae (1) and (2) amounts to 1% of the value of the first term, the value

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63.77

s/179/59/000/06/028/029 E031/E141

The Influence of Initial Section on the Hydraulia Resistance in Laminar Flow of Liquids in Tubes

L = 0.04d R

(3)

is found for the length of the local frictional section, agreeing with the findings of S.N. Targ for the length of the velocity of the initial section. The length of the mean frictional section is 26 times larger and is

 $L^0 = 1.044 R$ 

(4)

It follows from Eq (4) that Lo = 1040d for R = 203, so that in the majority of cases of leminar flow in tolers, Poiseuille's equation

= 6./R

(5)

is strictly speaking valid only for  $z \to \infty$ (when f = fo = (o), and corrections are required, Values of these corrections can be found from formulae (1) and (2). However, for practical calculations the expressions thus obtained are unsuitable, owing to the slow convergence of the corresponding series. For this reason the following simple approximate formulae are suggested for calculating the mean hydraulic resistance

Card 3/5

\$/179/59/000/06/013/019 \$081/\$J41

The Influence of Initial Section on the Hydraulic Resistance in Laminar Flow of Liquid in Tubes

coefficient:

Card 4/5

$$\Gamma^{\circ} = \left(\infty \left[1 + \frac{1}{96} \left(R \frac{d}{X}\right)\right] - \left(R \frac{d}{X}\right) \right) \left(\frac{E}{V} \infty = \frac{6L}{E}\right)$$

$$\Gamma^{\circ} = \left(\infty \cdot 30 \cdot 30 \cdot \left(R \frac{d}{X}\right)^{\circ} \cdot 10\right) \left(R \frac{d}{X} > 50\right) \quad (6)$$

Equations (6) cover practically all the useful range of the parameter Rd/x from 0 to 1000, in which the maximum error of approximation does not exceed 3%. For comparison we give the results of calculations for (1/1/100 by the available formulae and also by formula (6) for various Reynolds numbers

Rd/x = 1 10 20 50 100 200 500 1000

\$/179/59/000/06/028/02) BUSI/E1-1

The Influence of Initial Section on the Hydraulic Resustance in Laminar Flow of Liquids in Tuess

> (1.02 1.22 1.44 1.97 2.55 3.30 5.05 7.19 (Smiller-Boussinesq. Raf 2) 1.00 1.07 1.26 1.52 1.00 1,00 (Frenkel, Ref 5) 1,22 1.72 1.39 2.49 3.60 -.77 1.10 (Pormata (61)

There are 5 references, as follows:

- Shiller, L. Movement of liquid in tubes, OWII, 1936.
   Present State of hydrodynamics of viscous liquids, Vol 1, IL, 1958.
   Prandtl', L. Tit'ens. O. Hydrom and aeromechandus. Vol 2, ONTI, 1935.
- 4) Torg. S.M. Basic problems of the theory of Laurea. flow. GTTI, 1951.

5) Frenkel', N.Z. Hydraulics.

This is a complete translation

SUBMITTED: April 13, 1959

Card

5/5

## "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

10(4)

SOV/170-59-6-18/20

AUTHOR:

Sidorov, E.A.

TITLE:

On the Calculation of Hydraulic Resistance in the Initial Section

of Pipes Under Turbulent Conditions

PERIODICAL:

Inzhenerno-fizicheskiy zhurnal, 1959, Nr 6, pp 111-115 (USSR)

ABSTRACT:

In order to investigate the effect of the initial section of a pipe on hydraulic resistance, the author writes down equations of mass and moment conservation in dimensionless form. He makes use of the results of two experimental findings: 1. One of them expresses the law of velocity distribution over the cross section of a boundary layer, and 2. The second is the statement that the character of development of a boundary layer in the initial section of a pipe is similar to the character of development of a boundary layer, when a liquid flows around flat surfaces. The boundary conditions are obtained for the distribution of surface tension, cf, and the coefficient of hydraulic resistance along the length of a pipe f, and the problem is reduced to a system of six algebraic equations. The solution of this system yields the expressions for average

Card 1/2

SOV/170-59-6-18/20

On the Calculation of Hydraulic Resistance in the Initial Section of Pipes Under Turbulent Conditions

> hydraulic resistance, Formulae 15 and 16, and the values of relative coefficient of hydraulic resistance, plotted versus the values of

pipe length, are shown in Figure 1.

There are: 1 graph, 1 table and 11 references, 10 of which are

Soviet and 1 German.

ASSOCIATION: Energeticheskiy institut AN SSSR (Power Engineering Institute of

the AS USSR), Moscow.

Card 2/2

69912 \$/024/59/000/06/023/028 E032/1214

10,4000

(Moscow) Sidorov, E. A.

Generalization of the Grets Solution to the Case of AUTHOR:

Radiative Heat Transfer TITLE:

Izvestiya Akademii nauk SSSR, Otdeleniye PERIODICAL:

tekhnicheskikh nauk. Energetika i avtomatika, 1959,

Nr 6, pp 183-185 (USSR)

ABSTRACT: Grets (Ref 1) has given a solution of the problem of convective heat transfer in the case of laminar flow of liquids in stabilized sections of tubes at The differential equation for the heat transfer, which does

not take into account radiative terms, is given by Eq (1), where T(r, z) is the absolute temperature of the liquid, r and z are the radial and axial cylindrical coordinates, a is the reduced thermal conductivity (i.e. the ratio of the thermal conductivity and the product of the specific heat and the density of the medium), and v(r) is the velocity of the liquid. Grets has found solutions of Eq (1) for two cases,

namely, when the velocity distribution is parabolic (Eq (2)), and when it is constant (Eq (3)). However, it can be shown (Ref 2) that provided the condition Card 1/4

69942 \$/024/59/000/06/023/028 E032/E214

Generalization of the Grets Solution to the Case of Radiative Heat Transfer

2RP/z < 15 is satisfied (and it is satisfied in many practical cases), the two solutions are almost identical. The present author assumes In this condition P = 2UR/a. that this condition is satisfied and writes down the energy equation in the form given by Eq (5), in which radiation effects are included in the form of the second term on the right-hand side of Eq (5). In this equation,  $\rho$ , c and  $\lambda$  are the density, specific heat and thermal conductivity of the liquid,  $k=3\alpha/2$ , and φ is defined by the fourth equation on p 184 in which D = 2R is the diameter of the tube,  $\sigma$  is Stefan's constant, and n is the refractive index. Eq (5) is then linearized using the substitution given by Eq (6), where  $T_m$  is given by Eq (7) and  $T_0$  and  $T_1$  are the temperatures of the liquid at the input and of the walls of the tube respectively. The equations are then transformed into a dimensionless system of coordinates, which is defined by the relations immediately above Eq (8). When this substitution is carried out, the heat transfer

Card 2/4

69942

S/024/59/000/06/023/028 E032/E214

Generalization of the Grets Solution to the Case of Radiative Heat Transfer

equation can be rewritten in the form of Eq (8), the boundary conditions being

 $\theta = 0$  when x = 0  $\theta$  finite when y = 0 $\theta = 1$  when y = 1

The temperature distribution is then given by the last equation on p 184 in which  $J_0$ ,  $J_1$  and  $I_0$  are the ordinary and modified cylinder functions, and  $\beta_i$  are the roots of the equation  $J_0(x) = 0$ . For a transparent medium (B tending to zero), when the radiation can be neglected, one obtains the solution given by  $E_q$  (11) which is the same as that obtained by Grets for purely convective heat transfer. The total heat flux q passing through the walls of the tube (per unit area) can be found from Eq (11) and is given by Eq (12). An important consequence of Eqs (10) and (12) is the fact that when radiative corrections are brought in, the temperature drop and the quantity of heat given up by the medium change more

Card 3/4

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S/024/59/000/06/023/028 E032/E214

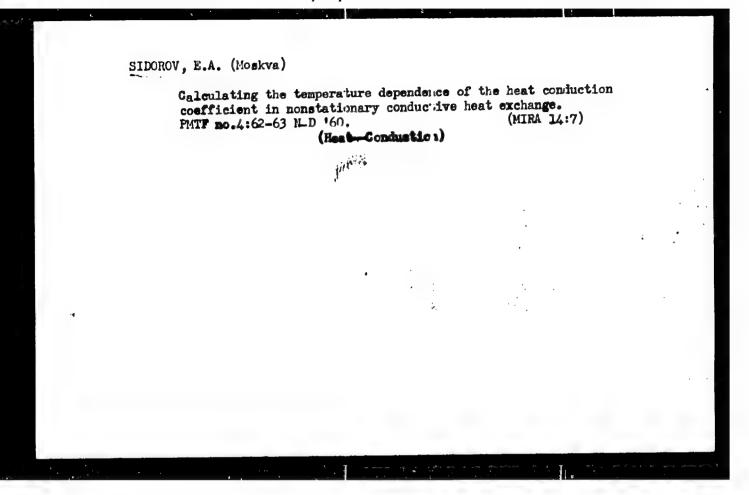
Generalization of the Grets Solution to the Case of Radiative

rapidly along the length of the tube as compared with the case when the correction is not included. There are 4 references, 3 of which are Soviet and 1 English.

SUBMITTED: June 2, 1959

4

Card 4/4



s/170/60/003/005/012/017 BO12/B056

AUTHOR:

Sidorov, E.

TITLE:

Calculation of the Combined Heat Interaction Between Solid

and Liquid Wedia

PERIODICAL:

Inzhenerno-fizicheskiy zhurnal, 1960, Vol. 3, No. 5,

pp. 106-110

TEXT: Approximation methods for the calculation of non-steady heat exchange are given. The problem to be solved is the following: An opaque solid of arbitrary shape, round which a liquid (or gas) flows, and which has the absolute surface temperature T, the integral degree of blackness & and the heat-transfer coefficient a is assumed. V is the velocity and To the absolute temperature of the thermally not disturbed part of the liquid flow. q is the density of the heat flux due to radiation from outside (upon the surface of the solid). As a result of the complicated heat exchange, the resulting heat flux q passes through the unit of the body

surface. It is assumed that the thermophysical properties of the liquid (or gas, respectively) and of the solid (o not depend on temperature. The Card 1/3

APPROVED FOR RELEASE: 08/23/2000

CIA-RDP86-00513R001550510007-7"

Calculation of the Combined Heat Interaction Between Solid and Liquid Media

S/170/60/003/005/012/017 B012/B056

functional interrelation between V,  $T_0$ ,  $q_0$ ,  $T_1$ , and  $q_1$  is sought. First, the heating of the body by radiation without convection is investigated. In this case, only the interrelation between  $q_0$ ,  $T_1$  and  $q_1$  need be found.

The formula (1) for thermal conductivity is written down, and it is shown that consideration of heat transfer by radiation leads to the nonlinear boundary condition (5). As a concrete example, the heating of a plane, rather thick wall by radiation is investigated. The thickness of the wall makes it possible to regard it as a semi-limited body during the time of investigation. If internal sources for heat production should be lacking, the differential equation (6) may be written down, for which the boundary conditions (7), (8), and (9) are given. Assuming formula (13), the boundary condition (8) is linearized, and formulas (17), (18), (19), and (20), which determine the required interrelation between q<sub>0</sub>, T<sub>1</sub>, and q<sub>1</sub>, are derived.

Next, the convective heat exchange is investigated in consideration of radiation. For this case, the approximate formula (24) is recommended, where the nonlinear boundary condition (5) becomes formula (25). In the present case, the solution of equation (1) makes it possible to determine the interrelation between  $q_1$ ,  $T_1$ ,  $q_0$ , and  $T_0^*$ ,  $\alpha = \alpha(V)$  is assumed to be Card 2/3

Calculation of the Combined Heat Interaction Between Solid and Liquid Media

S/170/60/003/005/012/017 B012/B056

known. In conclusion, the flow round a body of a great transverse thickness is investigated as an example. In this case, the body may be looked upon as a plane wall of unbounded thickness. There are 5 references: 4 Soviet and 1 British.

ASSOCIATION:

Institut teplofiziki 30 AN SSSR

(Institute of Heat Physics of the SO AS USSR)

Card 3/3

## "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

16.8000,21.1320,24.5200

78327 207/89-8-3-12/32

AUTHOR:

Sidorov, E. A.

TITLE:

Choice of Coolant for Nuclear Reactors. Letter to the

Editor

PERTODICAL

Atomnaya energiya, 1960, Vol 8, Nr 3, pp 252-254 (USSR)

ABSTRACT:

The author analyzed various coolants from the standpoint of heat-transfer and energy used in transporting the material. The goal was to bring the existing data by Goodman up to date by using more recent information by Vargaftik (Teplofizicheskiye svoystva veshchestv, Spravochnik (Thermal Properties of Materials, Manual) edited by Vargaftik, M., Gosenergoizdat, 1956) and Mikheyev (Osnovy teploperedachi (Introduction to Heat-Transfer) M., Gosenergoizdat, 1956). To compute the heat-transfer coefficients of heat carriers of the first class (liquids and gases with the Prandtl number Pr > 1) the author used the equation valid for the stabilized

turbulent flow:

Card 1/5

Choice of Coolant for Nuclear Reactors. Letter to the Editor 78327 sov/89-8-3-12/32

 $\alpha = 0.023C\lambda Pr^{0.4}v^{-0.8}$ 

(1)

where C depends on the construction of the heat exchanger, and  $\lambda$  and  $\nu$  are coefficients of heat conduction and kinematic viscosity, respectively. For the second class of carriers, representing liquid metals  $(Pr = 10^{-2} \text{ to } 10^{-4})$ , the author uses the approximate equation:

 $\alpha = 0.025C\lambda P_{P}^{\theta, \theta} v^{-0.8}$  (3)

Table 1 contains the result of the computations. The author also develops an expression for the dimensionless economic coefficient of heat-transfer which is equal to the ratio of the heat energy transferred by a particular

Card 2/5

Choice of Coolant for Nuclear Reactors.

Letter to the Editor

78327 80V/89-8-3-12/32

Table 1. Heat-transfer coefficients for various heat carriers. (a) heat carrier; (b) heat-transfer coefficient (relative unit--2.8 kcal·sec<sup>0.8</sup>/m<sup>2</sup>·h·deg) at temperatures in °C; (c) air; (d) carbon dioxide; (e) water vapor (on saturation curve); (f) water (on saturation curve); (g) dowtherm (liquid biphenyl mixture); (h) saltpeter mixture (melted salt); (i) mercury; (J) alloy (25% Na + 75% K); (k) sodium; (melted salt); (i) mercury; (J) alloy (25% Na + 75% K); (b) bismuth.

.) alloy (	70.5% BI + # 1:2%. E. 27.			161		
!	(a.)	Ion	200	300	iuo	500
ard 3/5	(C) (p=1 asm) (d) (p=1 asm) (k) (f-; (G) (h) (k) (k) (k) (k) (k) (n)	1,0 1,2 1,0 1,0-10 <sup>3</sup> 1,2-10 <sup>3</sup> 8,9-10 <sup>2</sup>	0,9 1,1 10 1,2-10 <sup>9</sup> 1,6-10 <sup>2</sup> 2,3-10 <sup>2</sup> 1,3-10 <sup>3</sup> 1,3-10 <sup>3</sup> 1,1-10 <sup>3</sup> 1,8-10 <sup>3</sup>	0,8 1,1 70 1,2-10 <sup>3</sup> 2,2-10 <sup>3</sup> 3,0-10 <sup>2</sup> 1,3-10 <sup>3</sup> 1,2-10 <sup>3</sup> 1,1-10 <sup>3</sup> 1,8-10 <sup>3</sup> 1,6-10 <sup>3</sup> 1,1-10 <sup>3</sup>	0,7 1,0 2,5-10 <sup>2</sup> 3,3-10 <sup>2</sup> 7,3-10 <sup>3</sup> 1,2-10 <sup>3</sup> 1,0-10 <sup>3</sup> 1,8-10 <sup>3</sup> 1,5-10 <sup>3</sup> 1,1-10 <sup>3</sup>	0,7 1,0 == 2,0 · 10 <sup>3</sup> 3,2 · 10 <sup>3</sup> 7,0 · 10 <sup>3</sup> 1,1 · 10 <sup>3</sup> 1,8 · 10 <sup>3</sup> 1,5 · 10 <sup>3</sup> 1,2 · 10 <sup>3</sup>

## "APPROVED FOR RELEASE: 08/23/2000 CIA-RDP86-00513R001550510007-7

Choice of Coolant for Nuclear Reactors. Letter to the Editor 78327 **SOV/89-8-3-12/3**2

coolant to the mechanical energy needed for its transport through tubes. Computed results are tabulated in Table 2. The final choice of coolant should, of course, also take into account other technical and economic factors, e.g., corrosion effects, stability, etc. There are 2 tables; and 4 references, 3 Soviet, 1 U.S. The U.S. reference is: Scientific and Technical Foundations of Nuclear Power Production, C. Goodman (ed.), M., Izd-vo inostr. lit., 1948-1950, Vol 1, p 287; Vol 2, p 124.

SUBMITTED:

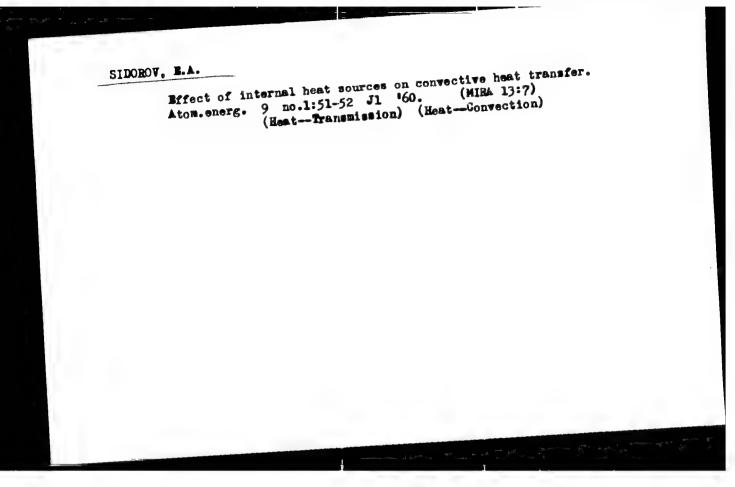
December 18, 1958

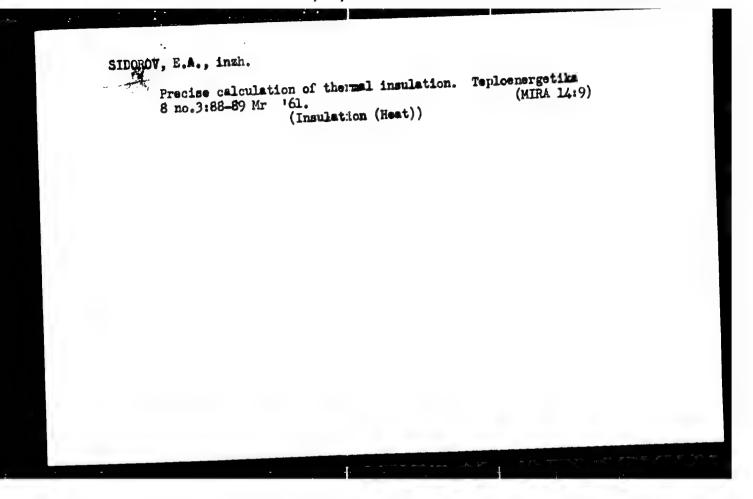
4/5

# "APPROVED FOR RELEASE: 08/23/2000

## CIA-RDP86-00513R001550510007-7

better to t	Table 2. E  Table 2. E  various hea  heat-transf  1.05   tom/m  same a. in	konomic t carrie: er coeff .1.h.der	roelficter. (a) Lolents . at ter	(nolati	ve un1t-	43 ⊬ca	T.360
	Diffue: Are			( <b>6</b>	, )		
	(a)		ţn i	190	778418	, 2710	1400 ·
	(() (p 1 utm)  (d) (p 1 atm)  (b)  (b)  (b)  (b)  (b)  (b)  (b)  (	m.)	1,0 0.9 1,7 2,9 0,33 2,4	1,0 0,9 213 4,6 0,18 0,17 0,37 2,6 0,37 0,31 7,2	1,0 1,0 3,8 5,8 0,28 0,20 0,39 2,6 0,37 0,33 7,7 0,46 0,36	1,0 1,1 0,35 0,37 2,6 0,39 0,31 8,0 0,68 0,39	1,0 1,1 0,37 0,41 2,7 0,39 0,37 8,2 0,70 0,41





s/170/63/006/002/018/018 B108/B186

26.5200

Sidorov, E. A.

AUTHOR:

The critical diameter of a spherical heat insulator

TITLE:

Inzhenerno-fizioheskiy zhurnal, v. 6, no. 2, 1963, 131-132

PERIODICAL:

TEXT: The critical diameter, i.e. that diameter at which the heat resistivity has a minimum, is calculated for a spherical heat insulator, the dependence of the coefficient  $\alpha_{\chi}(x)$  of convective heat transfer on

the diameter of the sphere being taken into consideration. the ratio of the variable outer diameter D of the insulation to the constant inner diameter d. The heat resistance of a spherical body is The relation Nu = ARe was found

 $\int (1 - 1/x)/2\lambda + 1/\alpha_x dx^2$ experimentally for convective heat transfer (B. D. Kantsel'son, F. A. Timofeyeva. Trudy Tsentral'nogo kotloturbincogo instituta (Proceedings of the Central Bouler and Turbine Institute), v. 12, no. 3, Mashgiz, 1949). n = 0 and A = 2 for Re < 10. With increasing Re, n increases from n = 0 (Re  $\rightarrow$  0) to n = 1 (Re  $\rightarrow \infty$ ).

Card 1/2

SITCHEV, D.A.

Considering the offect of some factors on near and mass transfer during turbulent them of compressible gas in underground gas producers. Hauth.trudy VMIII odsemgaza no. 10:10-21 463.

Sign figures of coefficients of the exponential law coessing or ig and boat and mass transfer in calculations of the and report georgic arter process. This.RI-24

Calculation of heat losses due to heat transfer in an underground gas generator. | 1511.174-12 (MIRA 1715)

1. Literatoriya merodinamicheskaya Vsesoyuzango mauchro-isaletovnieliskogo instituta poizemnoy gazifikatsit ugley.

The later - .; district the igniting of underground gas producers in lean cost sector. Their While casemaza no.12:27-32 '64. (MTRA 18:9)

1. Laboratoriya aeradinamicheskaya Vsosoyuznogo nauchno-issledovatel's per imminute podseenny gazifikatati ugley.

SIDOROV, E.A.

Calculation of the oxygen zone in a cylindrical carbon channel. Nauch. trudy VNIIPodzemgaza no.8:21-26 62. (MIRA 16:6)

1. Laboratoriya aerodinamicheskaya Vsesoyuznogo nauchnoissledovatel skogo instituta podzemnoy gazifikatsii ugley. (Coal gasification, Underground)

SIDOROV, E.A.

Methods of calculating the unidimensional gas flow in an underground gas producer channel with high temperatures and rates of flow. Trudy VNIIPodzemgaza no.12:32-25 164. (MIRA 18:9)

1. Laboratoriya aerodinamicheskaya Vsesoyuznogo nauci.noissledovatel'skogo instituta podzemnoy gazifikatsii ugley.

E. C. SIDOROV

Abs Jour

USSR/Zooparasitology - General Problems

: Ref Zhur - Biol., No 3, 1958, 10029

: Sidorov, E.G. Author

: Fish Parasites of Irgis-Turgay Basin Water Reservoirs. Inst

Title

Sb. rabot po ikhtiologii i gidrobiol. No 1, Alma-Ata, Orig Pub

1956, 232-251

In the summer of 1953 on Lake Dzhalangash 126 fish of six species, and on Lake Su-Thargan 268 fish of five species Abstract

were dissected. 45 species of parasites were found: 3 protozoa, 10 monogenetic trematodes, 16 digenetic, 5 cestodes, 5 nematodes, 2 "skreben" 1 leech, and 2 species of parasitic crustacea. The qualitative and quantitative wealth of ichthyoparasitofauna depends upon good attemperation of the lakes, mass development of plankton and

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benthos, and high density of fish population. A wide dis-

tribution of trypanosomes and a great variety of

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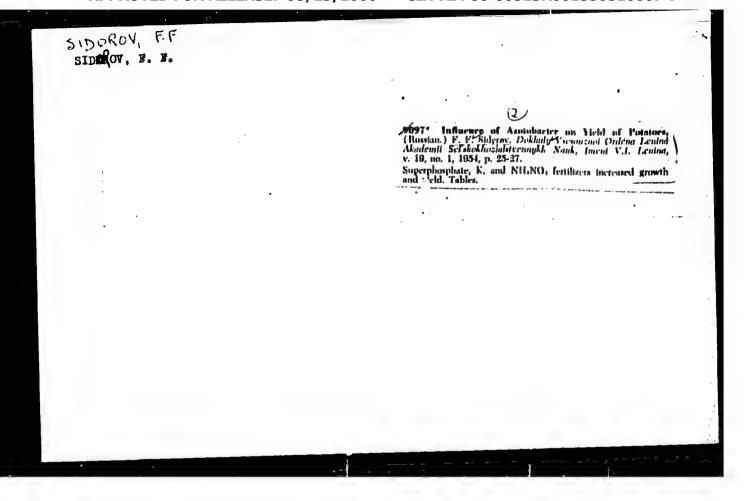
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full down, brittleness of the stalk, duration of the period

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between the emergence of shoots and flowering and of the period between flowering and maturiby of the spedices, ability of the plant to produce well-leveloged poller. An estimation is also given of the combination value of the colf-pollinating lines. The results attained on 130 lines are drawn up in a table. Materials are also given on the origin of the 73 self-pollinating lines must also ly used in selection and seed production.

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Inst : Wold Corn Collection at the Institute of Horticulture. Title

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COUNTRY : USSR

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ABS. JOUR. : RZhBiol., No. 1958 No. 104639

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INST. : TITLE : Some Biological Characteristics of the Davelopment in Corn.

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ABSTRACT : Results of the studies (in Leningrad oblest\*) of the pro-

cesses in the formation of inflorescences, leaves, and stems in different varieties. One part of the plants of each variety was raised with natural day illumination, the other - with a short, 10-hour day. With the shortened day of illumination, the number of leaves decreases and the height of the plants declines. Under the conditions of a normal day, the plants developed a larger number of leaves

and a longer stem. During this, the differences among the

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